

Jeffreys' Porridge Problem

"If porridge is cooked in a single saucepan and not stirred it will burn at the bottom. It can still be poured – it is still liquid, but at a certain stage of stickiness convection currents can be prevented even when the bottom is some hundreds of degrees hotter than the top." (Jeffreys 1957, Sir H. Jeffreys Papers C17)

Thermal convection in viscoplastic fluid is important in many industrial and geophysical applications. Jeffreys (1952, The Earth, C.U.P.) and other geophysicists in thinking of convection in the Earth's mantle, were among the first to appreciate that a finite fluid strength would substantially affect convection (e.g. Griggs 1939, Am. J. Sci. 237, 611; Orowan 1965, Phil. Trans. Roy. Soc. A, 258, 284). Orowan showed particular insight, suggesting that thermal convection would not readily initiate if the fluid has a yield stress, but that the Newtonian solution is a reasonable approximation once convection is underway.

Thermal convection in Newtonian fluids (the Rayleigh-Bénard problem) is a classic example of instability theory and pattern formation. Here we map out the corresponding problem for viscoplastic fluids. Unlike in the Newtonian fluid, the motionless conduction state is linearly stable for all Rayleigh number because the yield stress cannot be overcome by an infinitesimal perturbation (Zhang, Frigaard & Vola 2006, J.F.M., 566, 389). Can fluid microsctructure be broken with a finite kick to initiate convection?

Mathematical model

In the dimensionless formulation of the convection problem, the fluid depth, d, and thermal conductivity, κ , are used to build units for length, speed and time, and the temperature difference across the plates scales temperatures.

In terms of a streamfunction, $\psi(x, z, t)$, satisfying $(u, w) = (-\psi_z, \psi_x)$, and a temperature perturbation, $\theta(x, z, t)$, the equations are, assuming large Prandtl number, $\nu/\kappa \gg 1$

$$0 = \nabla^4 \psi + R\theta_x + \mathcal{B}$$

$$\theta_t + \psi_x \theta_z - \psi_z \theta_x = \nabla^2 \theta + \psi_x,$$

 $R = \text{Rayleigh number}, \nu = \text{kinematic viscosity}$ \mathcal{B} denotes the contribution from the non-Newtonian part of the stresses, $\hat{\tau}_{ik}$:

$$\mathcal{B} = \frac{\partial^2 \check{\tau}_{xz}}{\partial x^2} - \frac{\partial^2 \check{\tau}_{xz}}{\partial z^2} - 2\frac{\partial^2 \check{\tau}_{xx}}{\partial x \partial z},$$

The Bingham Fluid

Dimensional deviatoric stresses :
$$\boldsymbol{\tau} = \left(\rho\nu + \frac{\tau_y}{\dot{\gamma}}\right) \dot{\boldsymbol{\gamma}}, \text{ if } \tau_y < \boldsymbol{\tau}$$

and $\dot{\gamma}_{ik} = 0$ otherwise, where the deformation rates are

$$\dot{\boldsymbol{\gamma}} = \begin{pmatrix} -2\psi_{xz} & \psi_{xx} - \psi_{zz} \\ \psi_{xx} - \psi_{zz} & 2\psi_{xz} \end{pmatrix}, \qquad \dot{\gamma} = \sqrt{4\psi_{xz}^2 + (\psi_{xx} - \psi_{zz})^2}$$

FIG. 1: The Bingham model

$$\nu = \text{kinematic viscosity},$$

 $\tau_y = \text{yield stress. } \rho = \text{density.}$
Dimensionless yield stress : $B = \frac{\tau_Y d^2}{2}$.

The dimensionless yield stresses, $\hat{\tau}_{ik} = B \dot{\gamma}_{ik} / \dot{\gamma}$, lead to the non-Newtonian contribution,

 $\rho\nu\kappa$

$$\mathcal{B} = B \left[4 \left(\frac{\psi_{xz}}{\dot{\gamma}} \right)_{xz} + (\partial_x^2 - \partial_z^2) \left(\frac{\psi_{xx} - \psi_{zz}}{\dot{\gamma}} \right) \right].$$

THE BINGHAM-RAYLEIGH-BÉNARD PROBLEM

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